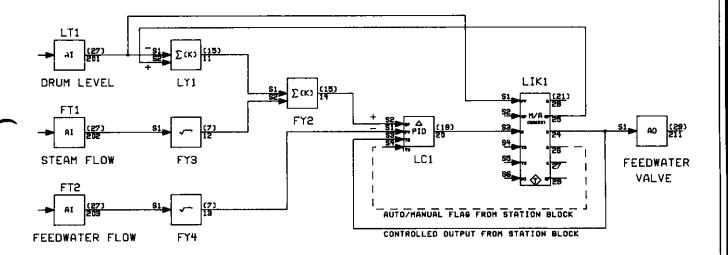
# Bailey® **Command Series**™

## **Loop Command Application Notes**



8020101A

## **Bailey Controls**

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#### **INTRODUCTION:**

This document is intended to show typical configurations which can be used to achieve a number of different control actions in a Bailey Loop Command Controller. The configurations shown are intended to serve as guidelines to aid in the configuration process. They can be used in conjunction with other configurations or as a starting point for the development of other control loops.

The first part of this document contains the various function codes needed to make the following configurations. A general description of the function code is included along with the description of its various specifications. Also a description or an explanation of the application is included.

The second part of the document has twelve control algorithms. There is a short description of each application, a process drawing and the Loop Command function block drawing of the configuration.

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#### SYMBOLS:

The selection and interaction of control functions on the active modules is accomplished by configuring "function blocks"

A function block is merely an input or output, or an operation on an input or output. These function blocks are generic software control algorithms that can be used to perform specific tasks which require dedicated hardware in other types of systems. There are four types of function blocks.

- 1 Executive
- 2 System Constants
- 3 Input/Output
- 4 User Configurable

The Executive blocks contain parameters which affect the overall operation of the module

System constant blocks are analog and digital parameters such a 0, 1, and 100 0, which are used as inputs for other blocks. This eliminates the need to configure blocks with commonly used parameters.

The I/O blocks are fixed block addresses which correspond to a module's field inputs and outputs through termination units and field wiring

User-configurable blocks are not pre-assigned but, instead, may be set up by the user to perform a wide variety of functions to implement control logic Each Loop Command Controller has a pre-defined set of block addresses for selection

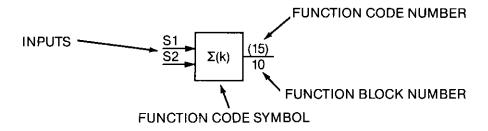
The process of defining module operations with function blocks is called configuration. To configure a function block, you must define the following parameters.

- Block Number
- Function Code
- Specification List

For example, a 2-input summer, Function Code 15, performs a weighted sum of two inputs. By choosing the proper gains and inputs this block can perform proportional, bias or difference functions. It can also be used as a scaler for a non-zero band signal by referencing the second input to a constant block. The operation of this function is described by the equation.

Output = 
$$\langle S1 \rangle$$
 (S3) +  $\langle S2 \rangle$  (S4)





#### **SPECIFICATIONS:**

S1 is block address of first input S2 is block address of second input S3 is gain parameter of input 1

S4 is gain parameter of input 2

(15) is function code number 10 is function block that function code 15 is assigned to  $\Sigma(k)$  is the symbol representing a summer with gain

#### **DATA RANGES**

DATA TYPE	RANGE	RESOLUTION
BOOLEAN	LOGIC 0 OR 1	N/A
INT(1)	0 TO 255	N/A
INT(2)	- 32,768 TO + 32,767	N/A
REAL(2)	$\pm 10 E - 03 TO \pm 40 E 06$	0 1%
REAL(3)	±27E - 20 TO ±92E 18	0 0015%

For more detailed information on each of the following function codes and how they are configured, please refer to the Bailey Function Code Application Manual, E93-900-20

#### LOOP COMMAND SYSTEM FUNCTION BLOCKS

BLOCK	USE
Logic Constants 0 1	Logic 0 Logic 1
Analog Constants  3 4 5 6 7 8 9 10 through 199 201 202 203 204 211 212 221 222 223 231 232 233	-100 0 -1 0 0 0 10 100 0 -9 2 E 18 9 2 E 18 User-Configurable Blocks (Analog or Digital) Analog Input 1 Analog Input 2 Analog Input 3 Analog Input 4 Analog Output 1 Analog Output 1 Digital Input 2 Digital Input 2 Digital Input 3 Digital Output 1 Digital Output 3 Digital Output 3
234 240	Digital Output 4 Executive Block (Function Code 53)

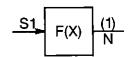
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#### **FUNCTION CODE 1**

#### **FUNCTION GENERATOR**

#### **GENERAL DESCRIPTION**

This function is used to approximate a non-linear output to input relationship. The input range is divided into five sections and a linear input to output realtionship is set up for each of those five sections. This function then computes an output which is related to the input according to those five linear relationships.



#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Output value of function

#### **SPECIFICATIONS**

SPEC NO.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1	NO YES	0 4 0 E 06	INT(2)	0 to 255 FULL	Block address of input Input coordinate
S2 S3	YES	0 000	REAL(2)/(3) REAL(2)/(3)	FULL	Output coordinate for S2
S4 S5	YES YES	4 0 E 06 0 000	REAL(2)/(3) REAL(2)/(3)	FULL FULL	Input coordinate   Output coordinate for S4
S6	YES	4 0 E 06	REAL(2)/(3)	FÜLL FÜLL	Input coordinate Output coordinate for S6
S7 S8	YES YES	0 000 4 0 E 06	REAL(2)/(3) REAL(2)/(3)	FULL	Input coordinate
S9 S10	YES YES	0 000 4 0 E 06	REAL(2)/(3) REAL(2)/(3)	FULL FULL	Output coordinate for S8 Input coordinate
S11	YES	0 000	REAL(2)/(3)	FULL FULL	Output coordinate for S10 Input coordinate
S12 S13	YES YES	4 0 E 06 0 000	REAL(2)/(3) REAL(2)/(3)	FULL	Output coordinate for S12

#### **EXPLANATION**

To set up this function, you must first determine what the output should be for a given range of input and draw a graph to show this relationship

The coordinates of the end points of these sections are then used as entries for specification S2 through S13. The even-numbered specifications are the X-axis coordinates and the odd-numbered ones are the Y-axis coordinates. This sets up a relationship such that when the X-axis input value is at S2, the output will be the value of S3 as shown in the graph. This actually divides the graph into five linear (straight-line) sections, each section having its own particular slope.

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#### **FUNCTION CODE 1**

If the input value is between two X-axis points, the output will be determined by the equation

Block Output = 
$$Y_{n-1} + \frac{(Y_n - Y_{n1})}{(X_n - X_{n1})} \times [X - X_{n-1}]$$

In this equation | X = the present input value

 $X_n$  = the X-axis specification point just above the present input value.

 $X_{n+1}$  = the X-axis specification point just below the present input value

 $Y_n$  = the Y-axis value that corresponds to  $X_n$ 

 $Y_{n,1}$  = the Y-axis coordinate that corresponds to  $X_{n,1}$ 

The  $[(Y_n - Y_{n\,1})/(X_n - X_{n\,1})]$  term is the slope of that particular graph segment (how much the output changes per input change)

The  $[X_n - X_{n+1}]$  term is the amount that the input is above the next lower specification point

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#### **FUNCTION CODE 3**

#### LEAD/LAG

#### **GENERAL DESCRIPTION**

In a block using this Function Code the output equals the product of some time function and the input value By using either S3 or S4 individually, either a lead or lag function is available. This function can also be used as a lead/lag filter.

## S1 F (t) (3) N

#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Output value with lead/lag function applied

#### **SPECIFICATIONS**

SPEC. NO.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1	NO	5	INT(2)	0 to 255	Block address of input Block address of Track Switch Signal 0 = track 1 = release
S2	NO	0	INT(2)	0 to 255	
S3	YES	0 000	REAL(2)/(3)	FULL	Time constant T1 (lead) sec Time constant T2 (lag) sec
S4	YES	0 000	REAL(2)/(3)	FULL	

#### **EXPLANATION**

This function code causes the output of the function block to lead or lag changes in the input signal. The operation is described by the equation

$$Y = Y_L + \frac{(S3) (\langle S1 \rangle - \langle S1_L \rangle)}{(S4) + dt} + \frac{dt (\langle S1 \rangle - Y_L)}{(S4) + dt}$$

where <S1 > = Present Input Value

<S1<sub>L</sub>> = Value of the Input on the Previous Cycle (S3) = Value of time constant T1 (lead) in seconds (S4) = Value of time constant T2 (lag) in seconds

Y = Present Output Value

 $Y_L = Value of the Output on the Previous Cycle$ 

dt = Module Cycle Time (seconds)

The S2 term enables or disables this function. If S2 is a logic 0, then the output will track the input, in other words, the output will be the same as the input at any given time. If S2 is set to a logic 1 level, the lead or lag function will be implemented.

#### Lag Function

If only a lag function is desired, S3 is left at its initial value (0) and a number is entered for S4. The equation then becomes

$$Y = Y_L + \frac{dt(\langle S1 \rangle - Y_L)}{(S4) + dt}$$

S4 is the time constant term and is defined as the time that it takes for the output of this function to reach 63 2% of the input value. The output will not reach approximately 99% of the input value until the end of five time constants. In this application, it will be five times S4 before the output to nearly equal the input in a certain number of seconds (t), the following equation can be used.

$$(S4) = \frac{t}{5}$$

In this equation

(S4) = the time contant term for Function Code 3

t = the number of seconds for the output to reach 99% of the input value

5 = the number of time constants required for the output to reach about 99% of the input value

For example, if it is required for the output to reach the input level in 30 seconds, the S4 term needed would be

$$S4 = \frac{t}{5} = \frac{30}{5} = 6$$

#### **Lead Function**

If only a lead function is desired, S4 is left at its initial value of 0 and a number is entered for S3. The equation then becomes

$$Y = Y_L + \frac{(S3)(\langle S1 \rangle - \langle S1_L \rangle) + dt(\langle S1 \rangle - Y_L)}{dt}$$

where

<S1 > = Present Input Value

 $\langle S1_1 \rangle = Value of the Input on the Previous Cycle$ 

(S3) = Value of time constant T1 (lead) in seconds

(S4) = Value of time constant T2 (lag) in seconds

Y = Present Output Value

Y<sub>L</sub> = Value of the Output on the Previous Cycle

dt = Module Cycle Time (seconds)

The output is set to the value that the input will be in S1 seconds if it continues to change at the same rate as it did during the last cycle. The lead function is essentially equal to the derivative function except that the Function Code 3 block output will eventually be the same as the input if the input remains constant long enough, while the output if a derivative function is zero when the input is not changing.

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#### **FUNCTION CODE 7**

#### **SQUARE ROOT**

#### **GENERAL DESCRIPTION**

This function computes the square root of the input signal in engineering units. The output equals a factor (K) times the square root of the input. The equation is

$$Y = S2\sqrt{\langle S1 \rangle}$$

where  $\langle S1 \rangle$  = Input value

S2 = Gain value (K) in engineering

units

Y = Output value Y = 0 if  $\langle S1 \rangle \leq 0$ 

#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Output value equals square root of input value multiplied by a scale factor

#### **SPECIFICATIONS**

SPEC. NO.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
\$1	NO	6	INT(2)	0 to 255	Block address of input
\$2	YES	1 000	REAL (2) /(3)	FULL	Gain value K in E U

#### **APPLICATIONS**

The Gain (K) can be any number used to scale an input signal to a meaningful or easy to work with output signal. Figure 7-1 shows an example of how Function Code 7 can be used. In this example, a flow rate of 0 to 50,000 lb/hr is being measured by a different pressure transducer whose output range is 0 to 200 "  $H_2O$  The flow is a function of the square root of the differential pressure multiplied by some constant (K). The equation for this is

Flow = 
$$K\sqrt{diff press}$$

Since it is known that the flow is 50,000 lb/hr at a transmitter output indicating 200" H₂O differential pressure, the required constant (K) can be calculated as follows

$$50,000 \text{ lb/hr} = \text{K}\sqrt{200}$$
  
 $50,000 \text{ lb/hr} = \text{K} (14 142)$   
 $\frac{50,000}{14 142} = \text{K}$   
 $\frac{14 142}{142} = \frac{14 142}{142}$ 

This value for K would be entered for S2 to implement this function



Many inputs are calibrated on a 0 to 100 scale. To ensure that outputs are also expressed in a linear 0 to 100 scale, a gain of 10 is commonly used.

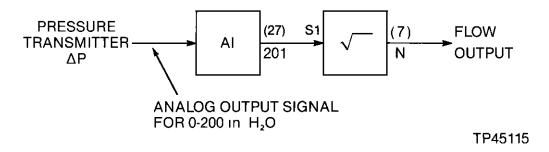


FIGURE 7-1 — Converting a Pressure Signal to a Flow Rate Using Function Code 7

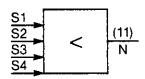
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## **FUNCTION CODE 11**

## **LOW SELECT**

#### **GENERAL DESCRIPTION**

This function selects and outputs the input with the lowest algebraic value



#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Output value equals the lowest of the four inputs

#### **SPECIFICATIONS**

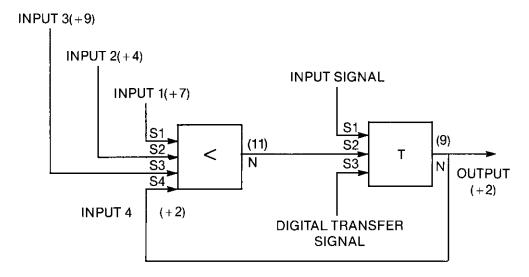
SPEC NO.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1 S2 S3 S4	NO NO NO	9999	INT(2) INT(2) INT(2) INT(2)	0 to 255 0 to 255 0 to 255 0 to 255 0 to 255	Block address of 1st input Block address of 2nd input Block address of 3rd input Block address of 4th input



#### **APPLICATIONS**

As well as selecting the lowest input value (common application) Function Code 11 can be used to memorize the lowest value over a period of time

To memorize the lowest value over a period of time, use Function Code 11 in conjunction with Function Code 9. This is shown in Figure 11-1. Create a loop with the output of Function Code 11 as an input to the Function Code 9 block and the output of Function Code 9 as an input to the Function Code 11 block. By selecting the output of the block executing Function Code 11 as the value that Function Code 9 tracks, you can feed the output of Function Code 11 back into Function Code 11, thus yielding the same value as the output of Function Code 11 for the period of time that it is the input with the smallest algebraic value.



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FIGURE 11-1 — Using Function Code 11 to Memorize a Low Value Over a Period of Time

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#### **FUNCTION CODE 15**

#### 2-INPUT SUMMER

Σ (K)

#### **GENERAL DESCRIPTION**

This function performs a weighted sum of two inputs By choosing the proper gains and inputs this block can perform proportional, bias or difference functions

It can also be used as a scaler for a non-zero based signal by referencing the second input to a constant block

The operation of this function is described by the equation

Output = 
$$< S1>(S3) + < S2>(S4)$$

#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Output value is the weighted algebraic sum of the two input signals

#### **SPECIFICATIONS**

SPEC NO	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1	NO	5	INT(2)	0 to 255	Block address of 1st input
S2	NO	5	INT(2)	0 to 255	Block address of 2nd input
S3	YES	1 000	REAL(2)/(3)	FULL	Gain parameter of input 1
S4	YES	1 000	REAL(2)/(3)	FULL	Gain parameter of input 2

#### **APPLICATIONS**

In addition to performing proportional, bias or difference functions, this code can also be used for scaling. By referencing the second input to one of the constant blocks or to a Manual Set Constant block (Function Code 2), a non-zero based signal can be scaled.

In the example shown in Figure 15-1 it is desired to scale an input with a range of 200 to 500 EU to give an output of 10 to 110 EU. The S3 constant can be calculated using the equation

$$S3 = \frac{\text{Output Span}}{< S1 > \text{Span}}$$
$$= \frac{110 - 10}{500 - 200} = 0.333$$



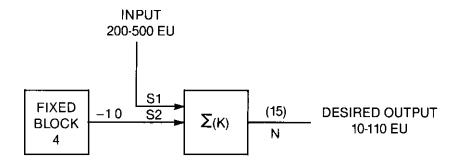
Fixed block 4 is entered for S2 to give it a constant value of -1.0 S2 could be set to any fixed value by using Function Code 2 but this approach requires more memory than using a fixed block. Since S2 and S4 are both constants in this example, they can be considered as a unit. The value for the product of <S2 > and S4 is determined from the equation.

$$\langle S2 \rangle (S4) = Output min -[\langle S1 min \rangle (S3 min)]$$

In this example then

$$\langle S2 \rangle (S4) = 10 - [(200)(0 3333)] = -56 667$$

<S2> and S4 could be set to any allowable values that will give the product of  $-56\,667$  In our example, <S2>is set to  $-1\,000$  so S4 would be set to  $56\,667$ 



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FIGURE 15-1 — Using Function Code 15 as a Scaler

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## **FUNCTION CODE 16**

#### **MULTIPLY**

#### **GENERAL DESCRIPTION**

This function performs a multiplication of <S1> by <S2> with the result multiplied by a constant S3

S2 X (16)

OUTPUT (EU) =  $(S3) \times (\langle S1 \rangle / \langle S2 \rangle)$ 

#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Output value is the weighted product of the two input signals

#### **SPECIFICATIONS**

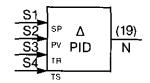
SPEC.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1	NO	6	INT(2)	0 to 255	Block address of 1st input
S2	NO	6	INT(2)	0 to 255	Block address of 2nd input
S3	YES	1 000	REAL(2)/(3)	FULL	Gain parameter



#### PID — PV and SP

#### **GENERAL DESCRIPTION**

This function provides proportional, integral and derivative action on an error developed from the PV (process variable) and SP (setpoint) inputs. The block has four inputs and one output. Besides the PV and SP inputs, there are also track reference and track switch input signals. If the track switch specification < S4 > is a logic 0, the output will follow the track reference signal specification < S3 > This provides a means for making smooth control transfers when the output of the PID controller is not being used as the control signal (such as when the loop is in "manual"). The parameters for the function block include an overall gain constant (S5), a proportional constant (S6), an integral constant (S7) and derivative gain constant (S8)



#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Output is PID signal in percent

#### **SPECIFICATIONS**

SPEC. NO	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1	NO	5	INT	0 to 255	Block address of process variable input
S2	NO	5 5	INT	0 to 255	Block address of set point
S3	NO	5	INT	0 to 255	Block address of track reference signal
S4	NO	1	INT	0 to 255	Block address of track switch signal 0 = track 1 = release
S5	YES	1 000	REAL(2)/(3)	FULL	(K) Gain multiplier
S6	YES	1 000	REAL(2)/(3)	FULL	(KP) Proportional contant
S7	YES	0 000	REAL(2)/(3)	FULL	(KI) Integral constant (1/min)
S8	YES	0 000	REAL(2)/(3)	FULL	(KD) Derivative constant (min)
S9	YES	105 000	REAL(2)/(3)	FULL	High output limit
S10	YES	-5 000	REAL(2)/(3)	FULL	Low output limit
S11	YES	0	BOOLEAN	0 or 1	0 = normal
S12	YES	0	BOOLEAN	0 or 1	1 = integral only (Kl NE 0) set point change 0 = reverse 1 = direct acting controller

#### **EXPLANATION**

This function operates in two modes — direct and reverse. The function is put in the direct mode when S12 is a logic 1 and in the reverse mode when S12 is a logic 0. In the direct mode the setpoint < S2> is subtracted from the process variable input < S1> and the output is obtained according to the following equation

DIRECT MODE S12 = 1

OUTPUT (%) = 
$$(\langle S1 \rangle - \langle S2 \rangle) \times [S5 \times (S6 + S7(I) + S8(D))]$$

where  $\langle S1 \rangle$  = Value of the Process Variable Input

<S2> = Value of Set Point Input
S5 = Value of Gain (K) multiplier

S6 = Value of Proportional Constant (KP)
S7 = Value of Integral Constant (KI) (1/min)
S8 = Value of Derivative Constant (KD) (min)
S12 = Controller mode identifier (direct or reverse)

In the reverse mode the process variable input <S1> is subtracted from the setpoint <S2> and the output is obtained according to the following equation

REVERSE MODE S12 = 0

OUTPUT (%) = 
$$( - ) \times [S5 \times (S6 + S7(I) + S8(D))]$$

The prime purpose of the main multiplier (S5) is to convert the difference signal (S1 - S2 or S2 - S1) from engineering units to a percentage so that the tuning constants (S6, S7, S8) can always be expressed in percentages. If the difference signal is in % (0 to 100%) the possible range of the error signal is -100% to 100%. The following equation is used to determine the gain multiplier (S5).

$$S5 = \frac{100}{\langle S1_{max} \rangle - \langle S1_{min} \rangle}$$

For example, with the function in the direct mode, if the range of the process variable signal is 0 to 200 cull ft/sec and the setpoint is 100 cull ft/sec, then S5 would be determined as follows

$$S5 = \frac{100}{\langle S1_{max} \rangle - \langle S1_{min} \rangle}$$

$$S5 = \frac{100}{(200 - 0)}$$

$$S5 = 5$$



#### M/A STATION (BASIC)

#### **GENERAL DESCRIPTION**

All three station functions (Basic, Cascade (Function Code 22), Ratio (Function Code 23)) provide an interface between the Controller module and the following interface devices the Digital Control Station (DCS), the Operator Interface Unit (OIU), the Management Command System (MCS), the Computer Interface Unit (CIU) and the faceplate on the Loop Command Controller

The Basic station generates a set point and provides Manual/Automatic transfers, Control Output adjustment in the Manual Mode, and set point adjustment in the Automatic Mode Specification S2 and S14 select the input the set point will track

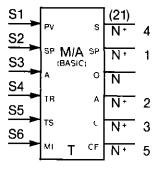
Other options include a Control-Output-Override input (S5) and a Manual-Interlock input (S6)

The Control-Output-Overide is used to force the Control Output value to a particular state (e.g., when the maintenance of a process safety requires immediate action)

The Manual-Interlock may be used to hold the station in Manual Mode, which allows conditional logic to be used to prevent automatic operations

#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Control output (CO) in percent (%)
N + 1	REAL	Set point in engineering units (EU)
N + 2	BOOLEAN	Mode 0 = manual 1 = automatic
N + 3	BOOLEAN	Level 0 = local 1 = computer
N + 4 N + 5	BOOLEAN BOOLEAN	Always 0 for basic station Computer backup indicates
		computer time out 0 = no 1 = yes



#### **SPECIFICATIONS**

SPEC.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
\$1 \$2 \$3 \$4	00000	5 5 5 5 0	INT(1) INT(1) INT(1) INT(1)	0 to 255 0 to 255 0 to 255 0 to 255 0 to 255	Block address of process variable input Block address of set point track value Block address of auto signal or input Block address of control output track signal (TR) Block address of track switch (TS)
S5 S6	NO NO	0	INT(1) INT(1)	0 to 255	0 = normal 1 = track Block address of manual interlock 1 = manual
\$7 \$8 \$9 \$10 \$11	YES YES YES NO NO	100 000* 0 000* 4 0 E 06* 100 000 0 000	REAL(2) REAL(2) REAL(2) REAL(2) REAL(2)	FULL FULL FULL FULL	Process variable high alarm point Process variable low alarm point Process variable set point deviation alarm point Signal span of set point and process variable Zero value of process variable
\$12 \$13 \$14	NO NO YES	0 000 0 0	REAL(2) INT(1) INT(1)	FULL 0 to 255 0 to 255	Zero value of set point EU identifier (Note for OIU and MCS use only) Set point track option 0 = no 1 = process variable 2 = S2/manual only
S15	NO	0	INT(1)	0 to 255	3 = S2/manual + auto Computer timeout option 0 = computer auto/manual mode unchanged 1 = computer manual 2 = computer auto 3 = computer cascade/ratio 4 = local auto/manual mode unchanged 5 = local manual
S16	NO	0	INT(1)	0 to 255	6 = local auto 7 = local cascade/ratio Digital control station address ( >15 indicated no station)

<sup>\*</sup> Not Adaptable

#### **EXPLANATION**

#### **Specifications**

- S1 PV Block Number whose output is the process variable. This input drives the Digital Station PV indicator (in Engineering Units)
- S2 SPT Block Number whose output the set point is to track, depending on S14 (Track Setpoint)
- \$3 COAUTO Block Number whose output value is the Control Output when the station is in auto mode (usually the output of a PID block)
- S4 COTRCK Block number whose output is used as the Control Output when the station is tracking (Control Output Override Mode) and also as the initial value for the Control Output on start-up
- S5 COFLG Block Number whose output value determines whether the Control Output is to be tracked. If the output of the block is
  - 0 = No Tracking (normal)
  - 1 = Track output of block specified by S4

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#### **FUNCTION CODE 21**

- S6 REMLOCK Block Number whose output value determines whether the station is locked in manual mode
  - 0 = No 1 = Yes
- NOTE Specifications S7, S8 and S9 are tunable but not adaptable
- S7 PVH Engineering Units (EU) value of PV at which a high alarm will be generated (displayed on the faceplate)
- S8 PVL EU value at which a low alarm will be generated and displayed on the faceplate
- S9 PVDEV EU value of allowed deviation between PV and SP A high deviation alarm is generated when the PV is greater than the SP and the value of the difference between the two is greater than or equal to this specification. A low deviation alarm generated when the PV is less than the SP and the value of the difference between the two is greater than or equal to this specification. These two alarm conditions are reported to the OIU and MCS only.
- \$10 EUSPAN Value corresponding to EU span for PV and SP
- S11 EUPVZ Value corresponding to EU zero percent for PV
- S12 EUSPZ Value corresponding to EU zero percent for SP
- \$13 EUID Engineering units type
- NOTE This data is used with OIU and MCS only
- S14 TRCKSP Value that determined which input the set point will track in Manual mode Selecting 3 causes set point tracking in both Manual and Auto modes
  - 0 = No Tracking
  - 1 = Track PV (S1)
  - 2 = Track SP (S2)
  - 3 = Track S2 always (Auto & Manual)
- S15 COMPDEF Value that determines the system default mode if the computer times out while the loop is under computer control
  - 0 computer auto/manual mode unchanged
  - 1 computer manual
  - 2 computer auto
  - 3 computer cascade/ratio (unused in Function Code 21)
  - 4 local auto/manual mode unchanged
  - 5 local manual
  - 6 local auto
  - 7 local cascade/ratio (unused in Function Code 21)
- S16 DIGSTAAD Value of the hardware digital station address that the station function block is representing. A number greater than 15 indicates no hardware station.

#### STATION OUTPUT EXAMPLE

A user has assigned block number 30 to a standard station. The system then assigns the next five block numbers as listed below. If the user needs to assign more block numbers after the station block, he must add 6 to the station's block number to obtain the next available block number.

BLOCK NO.	STATION OUTPUT	
30	CO	
31	SP	
32	MODE	
33	LEVEL	
34	STATION MODE	
34 35	COMPUTER BACKUP	
36	NEXT AVAILABLE	

In this manner, the user may specify each output of a station block by a unique reference number

#### **Control Output Tracking**

When the Control Output Track state (S5) is 1, it does not affect the output designation of the block but will override the current Control Output with the value in the block specified by S4. The actual operating state is saved, and will be restored when the track flag input goes to 0.

While the station is under Local Manual control, the output is expressed as a percentage from 0 to 100 percent. If the input to the station is a calculation function, the input value must be scaled to percent, and the output of the station scaled to the required value, external to the station.

When the Manual Interlock state (S6) is 1, the station is tripped to the Manual mode

#### **Set Point Tracking**

The set point may be adjusted from the faceplate only if set point tracking is not selected (0 for S14). If one of the tracking options is selected, the set point will be determined by the option chosen.



#### **EXAMPLES**

- S2 Number of block containing output the set point is to track in Manual mode
- S14 Set Point Track Option
  - 0 No tracking
  - 1 Track PV (S1) when station is in manual
  - 2 Track value in block selected in S2 in Manual mode only
  - 3 Track Value in block selected in S2 always (Auto and Manual)
    No direct control of set point from station
  - If \$14=0. The set point can be varied using local manual control
  - If S14=1 The set point will track the PV when the station is in Manual This provides bumpless transfer with the station is returned to Automatic mode. The set point cannot be varied manually in this mode.
  - If S2=Blk # and S14=2. The set point will track the value in the block specified in S2 when the station is in Manual Set point may be changed when the station is returned to Automatic mode bump in the set point value is possible when transferred to manual
  - If S2=Blk # and S14=3. The set point will track the value in the block specified in S2 when the station is in either Automatic or Manual mode. No direct set point adjustments can be made from the station.

#### 23:10:46 04/10/07

#### **FUNCTION CODE 22**

## M/A STATION (CASCADE)

#### **GENERAL DESCRIPTION**

The Cascade station provides all of the basic functions plus an additional mode that allows the set point to be controlled by another function block. When the station is in Cascade mode, the value found in the block specified by S2 will be the set point. In the Basic (non-cascade) mode, the set point signal is equal to the value set by the operator.

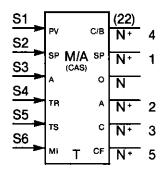
Other options include a Control-Output-Override input (S5) and a Manual-Interlock input (S6)

The Control-Output-Override is used to force the Control Output value to a particular state (e.g., when the maintenance of process safety requires immediate action)

The Manual-Interlock may be used to hold the station in Manual Mode, which allows conditional logic to be used to prevent automatic operations

#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Control output (CO) in percent (%)
N + 1	REAL	Set point in engineering units (EU)
N + 2	BOOLEAN	Mode 0 = manual 1 = automatic
N + 3	BOOLEAN	Level 0 = local 1 = computer
N + 4	BOOLEAN	Station Mode 0 = Basic, 1 = Cascade
N + 5	BOOLEAN	Computer backup indicates computer time out  0 = no 1 = yes



#### **SPECIFICATIONS**

SPEC.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1 S2 S3 S4 S5	NO NO NO NO	55550	INT(1) INT(1) INT(1) INT(1) INT(1)	0 to 255 0 to 255 0 to 255 0 to 255 0 to 255	Block address of process variable Block address of set point track value Block address of auto signal or input Block address of control output track signal (TR) Block address of track switch (TS)  0 = normal
S6	NO	0	INT(1)	0 to 255	1 = track Block address of manual interlock 1 = manual
\$7 \$8 \$9 \$10 \$11 \$12 \$13 \$14	YES* YES* YES* NO NO NO NO YES	100 000 0 000 4 0 E 06 100 000 0 000 0 000 0	REAL(2) REAL(2) REAL(2) REAL(2) REAL(2) REAL(2) INT(1) INT(1)	FULL FULL FULL FULL FULL FULL O to 255 0 to 255	Process variable high alarm point Process variable low alarm point Process variable set point deviation alarm point Signal span of set point and process variable Zero value of process variable Zero value of set point E U identifier (Note for OIU and MCS use only) Set point track option 0 = no 1 = process variable 2 = S2/manual only
S15	NO	0	INT(1)	0 to 255	3 = S2/manual + auto Computer timeout option 0 = computer auto/manual mode unchanged 1 = computer manual 2 = computer auto 3 = computer cascade/ratio 4 = local auto/manual mode unchanged 5 = local manual 6 = local auto 7   local accorde/ratio
S16	NO	0	INT(1)	0 to 255	7 = local cascade/ratio Digital control station address ( >15 indicated no station)

<sup>\*</sup> Not Adaptable

#### **EXPLANATION**

#### **Specifications**

- **S1** PV Block Number whose output is the process variable (Engineering Units)
  This input drives the Digital Station PV indicator
- S2 CASCADE Block address of Cascade input The output of this block is the set point when the station is in Cascade mode
- S3 COAUTO Block Number whose output value is the Control Output when the station is in auto mode (usually the output of a PID block)
- \$4 COTRCK Block Number whose output is used as the Control Output when the station is tracking (Control Output Override Mode) and also as the initial value for the Control Output on start-up
- S5 COFLG Block Number whose output value determines whether the Control Output is to be tracked
  - 0 = No
  - 1 = Yes

- **S6** REMLOCK Block Number whose output value determines whether the station is locked in manual mode
  - 0 = No 1 = Yes
- NOTE Specifications S7, S8 and S9 are tunable but not adaptable
- S7 PVH Engineering Units (EU) value of PV at which a high alarm will be generated (displayed on the faceplate and/or OIU or MCS)
- S8 PVL EU value of PV at which a low alarm will be generated
- S9 PVDEV EU value of allowed deviation between PV and SP A high deviation alarm is generated when the PV is greater than the SP and the value of the difference between the two is greater than or equal to this specification. A low deviation alarm generated when the PV is less than the SP and the value of the difference between the two is greater than or equal to this specification. These two alarm conditions are reported to the OIU and MCS only.
- S10 EUSPAN Value corresponding to EU span for PV and SP
- S11 EUPVZ Value corresponding to EU zero percent for PV
- S12 EUSPZ Value corresponding to EU zero percent for SP
- S13 EUIDENT Engineering units type
- NOTE This data is used with OIU and MCS only
- S14 TRCKSP Value that determines which input the set point will track in Manual mode Selecting 3 causes set point tracking in both Manual and Auto modes
  - 0 = No Tracking
  - 1 = Track PV (S1)
  - 2 = Track CASCADE (S2)
  - 3 = Track S2 always (Auto & Manual)
- S15 COMPDEF Value that determines the system default mode if the computer times out while the loop is under computer control
  - 0 computer (auto/manual mode unchanged)
  - 1 computer manual
  - 2 computer auto
  - 3 computer cascade
  - 4 local (auto/manual mode unchanged)
  - 5 local manual
  - 6 local auto
  - 7 local cascade
- \$16 DIGSTAAD Value of the hardware digital station address that the station function block is representing. A number greater than 15 indicates no Hardware Station.



## M/A STATION (RATIO)

#### **GENERAL DESCRIPTION**

The Ratio station provides Manual/Automatic transfers, Control Output adjustment in the Manual mode, and set point adjustment in the Automatic mode. It differs from the Basic and Cascade stations in its method of set point generation. A ratio adjustment is provided to control the measured variable in a ratio (R) to a second uncontrolled (wild) variable (S2). A Ratio/Basic switch provides the ability to operate as a set point station in the Basic position. Specifications S2 and S14 select the input the set point will track in the Manual Basic mode. In the Basic (non-ratio) mode, the set point signal is equal to the value set by the operator.

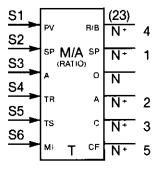
Other options include a Control-Output-Override input (S5) and a Manual-Interlock input (S6)

The Control-Output-Override is used to force the Control Output value to a particular state (e.g., when the maintenance of process safety requires immediate action)

The Manual-Interlock may be used to hold the station in Manual Mode, which allows conditional logic to be used to prevent automatic operations

#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Control output (CO) in percent (%)
N + 1	REAL	Set point in engineering units (EU)
N + 2	BOOLEAN	Mode 0 = manual 1 = automatic
N + 3	BOOLEAN	Level 0 = local 1 = computer
N + 4	BOOLEAN	Station Mode 0 = Basic, 1 = Ratio
N + 5	BOOLEAN	Computer backup indicates computer time out  0 = no 1 = yes



NOTE The maximum ratio is 10, the minimum practical ratio is 0.05

#### **SPECIFICATIONS**

SPEC. NO.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1	NO	5	INT(1)	0 to 255	Block address of process variable
S2	NO	5 5	INT(1)	0 to 255	Block address of set point track value
S3	NO	5	INT(1)	0 to 255	Block address of auto signal or input
S4	NO	5 5 0	INT(1)	0 to 255	Block address of control output track signal (TR)
l 55	NO	Ō	INT(1)	0 to 255	Block address of track switch (TS)
			<b>,</b> ,		0 = normal 1 = track
l se	NO	0	INT(1)	0 to 255	Block address of manual interlock
"	''•	Ū	(.,	0.10.200	1 = manual
S7	YES*	100 000	REAL(2)	FULL	Process variable high alarm point
l S8	YES*	0 000	REAL(2)	FULL	Process variable low alarm point
S9	YES*	40E06	REAL(2)	FULL	Process variable set point deviation alarm point
S10	NO	100 000	REAL(2)	FULL	Signal span of set point and process variable
S11	NO	0 000	REAL(2)	FULL	Zero value of process variable
S12	NO	0 000	REAL(2)	FULL	Zero value of set point
S13	NO	0	INT(1)	0 to 255	EU identifier (Note for OIU and MCS use only)
S14	YES	0	INT(1)	0 to 255	Set point track option
1					0 = no
					1 = process variable
					2 = S2/manual only
1		_			3 = S2/manual + auto
S15	NO	0	INT(1)	0 to 255	Computer timeout option
					0 = computer auto/manual mode unchanged
					1 = computer manual
					2 = computer auto
					3 = computer cascade/ratio
					4 = local auto/manual mode unchanged
					5 = local manual
					6 = local auto
0.10	NO	۸ ا	(NIT/d)	0 to 055	7 = local cascade/ratio
S16	NO	0	INT(1)	0 to 255	Digital control station address
			L	l	( > 15 indicated no station)

<sup>\*</sup> Not Adaptable

#### **EXPLANATION**

#### **Specifications**

- S1 PV Block Number whose output is the process variable. This input drives the Digital Station PV indicator (in Engineering Units)
- S2 WILD Block address of uncontrolled input. A multiple of the output of this block is the set point when the station is in Ratio mode.
- S3 COAUTO Block Number whose output value is the Control Output when the station is in auto mode (usually the output of a PID block)
- \$4 COTRCK Block Number whose output is used as the Control Output when the station is tracking (Control Output Override Mode) and also as the initial value for the Control Output on start-up
- \$5 COFLG Block Number whose output value determines whether the Control Output is to be tracked

0 = No

1 = Yes

## 23:10:50 04/10/07

#### **FUNCTION CODE 23**

- S6 REMLOCK Block Number of the Remote Interlock which determines whether the station is locked in manual mode
  - 0 = No
  - 1 = Yes
- NOTE Specifications S7, S8 and S9 are tunable but not adaptable
- S7 PVH Engineering Units (EU) value of PV at which a high alarm will be generated (displayed on the faceplate and/or OIU or MCS)
- S8 PVL EU value of PV at which a low alarm will be generated
- S9 PVDEV EU value of allowed deviation between PV and SP A high deviation alarm is generated when the PV is greater than the SP and the value of the difference between the two is greater than or equal to this specification. A low deviation alarm generated when the PV is less than the SP and the value of the difference between the two is greater than or equal to this specification. These two alarm conditions are reported to the OIU and MCS only.
- \$10 EUSPAN Value corresponding to EU span for PV and SP
- S11 EUPVZ Value corresponding to EU zero percent for PV
- \$12 EUSPZ Value corresponding to EU zero percent for SP
- S13 EUIDENT Engineering units type
- NOTE This data is used with OIU and MCS only
- S14 TRCKSP Value that determines which input the set point will track in Manual mode Selecting 3 causes set point tracking in both Manual and Auto modes
  - 0 = No Tracking
  - 1 = Track PV (S1)
  - 2 = Track WILD (S2)
  - 3 = Track S2 always (Auto & Manual)
- S15 COMPDEF Value that determines the system default mode if the computer times out while the loop is under computer control
  - 0 computer (auto/manual mode unchanged)
  - 1 computer manual
  - 2 computer auto
  - 3 computer ratio
  - 4 local (auto/manual mode unchanged)
  - 5 local manual
  - 6 local auto
  - 7 local ratio
- S16 DIGSTAAD Value of the hardware digital station address that the station function block is representing. A number greater than 15 indicates no Hardware Station.

#### 23:10:52 04/10/07

#### **FUNCTION CODE 24**

#### **ADAPT**

#### **GENERAL DESCRIPTION**

This function allows the adaptation of any tunable parameter in the system (Tunable parameters may be modified during execution) It is used to compensate for known dynamic loop gains in control schemes. All gains and time constants are tunable parameters, therefore, using this function, you can set gains and time constants to fit current process operating states.

The function block output value has no significance The specification is modified only during execution, and the original parameter that is stored in NVRAM is not modified. Thus, the revised specification is not accessible via any of the operator interface devices unless the ADAPT input is read. (Block inputs are read by reading the output of the block preceding the block of interest.)

#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N		See description

#### **SPECIFICATIONS**

SPEC. NO.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
\$1 \$2	NO NO	0	INT(1) INT(1)	0 to 255 0 to 255	Block address of input Address of Block containing spec to be adapted
S3	NO	0	INT(1)	0 to 255	Spec number of spec to be adapted



#### **APPLICATIONS**

Figures 24-1 and 24-2 show the input to an ADAPT block as the result of a function defined by Function Code 1. If the function varies with time, the adapted parameter also varies with time. The same is true for functions of pressure, temperature, tank level, etc. This arrangement makes variable control of tunable parameters possible, allowing the user to compensate for gains inherent in a process.

In Figure 24-1, the High output limit (S9) of a Function Code 19 block varies as a function of x as defined in a Function Code 1 block

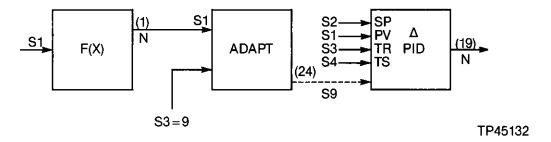


FIGURE 24-1 — Creation of a Sliding Limiter or Index With Function Code 24

In 24-2 an ADAPT block adapts the proportional constant (S6) of a Function Code 19 block to the value received from a Function Code 1 block, allowing the user to modify gain with changes in a specified parameter, x

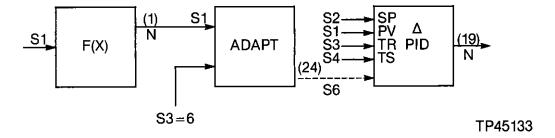


FIGURE 24-2 — Function Code 24 Used to Achieve Variable Controller Gain

#### 23:10:54 04/10/07

#### **FUNCTION CODE 27**

#### ANALOG INPUT

#### **GENERAL DESCRIPTION**

The ANALOG INPUT Function Code is used to acquire analog inputs from the termination unit for the Loop Command This function acts ONLY on Loop Command fixed inputs Analog input 1 will always be found in block 201, analog input 2 in block 202, etc To obtain this function, specify a fixed analog input block number (201-204) Zero and span values, expressed in engineering units, are defined by the specifications. If a span in 0.0, the input is defined as unused. Fixed blocks can be modified with the Configuration and Tuning Module (CTM), Configuration and Tuning Terminal (CTT), the Operator interface units (OIU) or the Management Command System (MCS)

A Point Quality flag is generated based on the analog signal. To test the quality of the signal, include a Function Code 31 (TEST QUALITY) block in your configuration. The quality of the point cannot be used as an input to any other type of block. The analog output value can be used as an input to any analog processing block.

#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
201	REAL	CLC fixed input Al #1 and Quality
202	REAL	CLC fixed input AI #2 and Quality
203	REAL	CLC fixed input Al #3 and Quality
204	REAL	CLC fixed input AI #4 and Quality

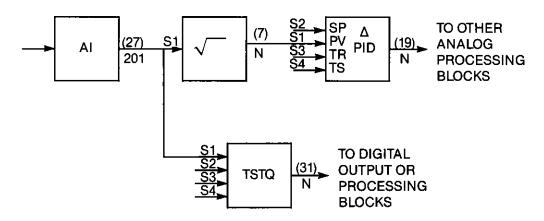
#### **SPECIFICATIONS**

SPEC. NO.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1	NO	0 000	REAL(2)	FULL	Signal zero in E U
S2	NO	0 000	REAL(2)	FULL	Signal span in E U



#### **EXPLANATION**

Figure 27-1 shows the use of a Function Code 31 block to test the quality of the output from the Function Code 27 block



TP45132

FIGURE 27-1 — Configuration Required to Test Point Quality

## 23:10:56 04/10/07

#### **FUNCTION CODE 30**

#### ANALOG EXCEPTION REPORT

#### **GENERAL DESCRIPTION**

The ANALOG EXCEPTION REPORT Function Code causes the input value to be sent on the plant loop if the time limit and/or significant change is exceeded. This function also generates an alarm if the high or low limit values are exceeded.

This function does not perform any conversion of input S3 and S4 (zero and span of input) are used internally for limits, and significant change is used for reporting to other Process Control Units or Operator Interface Devices The engineering units parameters are used only for reporting to these higher level devices

A Boolean point quality flag is generated based on the analog signal. To test the quality of the signal, you must include a Function Code 31 (TEST QUALITY) block in your configuration. You can also propagate quality if the input is from Function Code 137 (BASIC REAL OUTPUT). The quality of the point cannot be used as an input to any other type of block.

#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Analog Output Value and Quality Quality 0 = good, 1 = bad

#### **SPECIFICATIONS**

SPEC. NO.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1	NO	0	INT(2)	0 to 255	Block address of input
S2	NO	0 000	INT(2)	0 to 255	Engineering unit identifier
<b>S</b> 3	NO	0.000	REAL(2)/(3)	FULL	Zero of S1 input in EU
	NO	100	REAL(2)/(3)	FULL	Span of S1 input in EU
S4 S5	YES	100	REAL(2)/(3)	FULL	High alarm point limit value
S6	YES	0 000	REAL(2)/(3)	FULL	Low alarm point limit value
S7	NO	1 000	REAL(2)/(3)	FULL	Significant change (% of span)

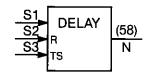
All alarm limits are tunable, but not adaptable



## **TIME DELAY (ANALOG)**

#### **GENERAL DESCRIPTION**

The TIME DELAY Function Code provides a pure delay on an analog signal. This function can be used to create fixed to variable time delays, or to model systems to represent dynamic time delays.



#### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Time delayed function of input

#### **SPECIFICATIONS**

SPEC. NO.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1	NO	0	INT(2)	0 to 255	Block address of input (X)
S2	NO !	6	INT(2)	0 to 255	Block address of rate input (R, in units/sec)
S3	NO	1	INT(2)	0 to 255	Block address of track switch signal  0 = track 1 = release
S4 S5	NO NO	0 000 1 000	REAL(2)/(3) INT(1)	FULL 0 to 255	Length of queue (L, in units) Number of intervals (N)

#### **EXPLANATION**

#### **Specifications**

\$1 <X> - Block address of input

\$2 <R >- Block address of rate input in units per second

S3 <T>-Block address of track switch signal <S3> = 0, track input, <S3> = 1, release When <S3> = 0, it initializes all N elements of the memory to the input value

Then  $M_1 = M_2 = M_N = \langle S1 \rangle$ , and elapsed time since the last sample = 0 There is no time delay

If 
$$\langle S3 \rangle = 1$$
, then

Time delay = 
$$\frac{S4}{< S2>}$$

Timing interval (TI) = 
$$\frac{\text{Time Delay}}{\text{S5}}$$

Elapsed Time = ET + t

where ET = time since last sample in seconds

t = time since last algorithm execution in seconds

TI = internal input sample in seconds

M<sub>1</sub> = Memory locations where input values are stored during

time delay

If ET ≥ TI

then,  $M_i = M_{i+1}$ , for i = 0 to N.

 $M_N$  = output value, and  $M_1$  =  $\langle S1 \rangle$ 

Elapsed time = ET - TI

- S4 L Length of the queue in units, The queue is the number of units over which the time delay is to be effective
- S5 N Number of Intervals Number of times from one to 190, that the input is to be sampled N is determined by dividing the time delay (TD) by the desired sampling frequency. See the Fixed Time Delay example.

### **APPLICATIONS**

### **Fixed Time Delay**

For a fixed time delay, the rate input, <S2>, is constant. The time delay between output and input varies only with S4. It is directly proportional to S4. Assume you wish to simulate the time delay for flow through a pipe. Assume a required time delay of two minutes with input sampling desired every five seconds. Select the default value of 1.0 (found in Fixed Block 6) for S2 since rate is constant for fixed delays.

<S2> = Rate in units per second = 10
S4 = Length of the queue in units

S5 = Number of intervals

Time Delay = 2 minutes = 120 seconds

TD = 120 seconds

TD =  $\frac{\$4}{\$2}$ 

 $120 = \frac{S4}{10}$ 

S4 = 120 units = Length of queue

For input sampling every five seconds

$$N = \frac{10}{5 \text{ sec}}$$

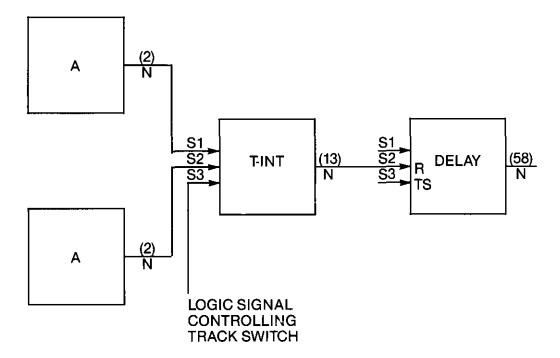
$$= \frac{120 \sec}{5 \sec}$$

= 24 intervals



### Variable Time Delay

Variable time delays may be dynamically adjusted by changing the value of S2 Using a Function Code 9 block, as illustrated in Figure 58-2, the user can switch between two fixed input rates. In the fixed time delay example, when <S2>=10, the time delay, S4/<S2>=120 seconds. If <S2>1s changed to 20, then the time delay becomes 60 seconds, and the timing interval, TD/N = 25 seconds. Changing the rate input <S2>1 while holding all other parameters constant changes the timing interval. Faster rates produce more frequent input sampling, and slower rates produce less frequent input sampling for the same number of intervals.



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FIGURE 58-2 — Function Code 58 Used for Variable Time Delay

### 23:10:59 04/10/07

### **FUNCTION CODE 152**

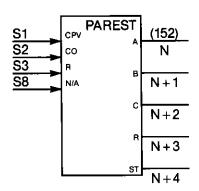
### MODEL PARAMETER ESTIMATOR

### **GENERAL DESCRIPTION**

The Model Parameter Estimator function block uses a recursive least-squares algorithm to identify a mathematical model of a process. This function block calculates the parameters for a linear, first-order dynamic model with deadtime of the specific form.

$$Y(t) = a * y(t-1) + b * u(t-k) + c$$

This function continuously monitors the value of the controlled process variable and the control output. The value of the model parameters is calculated whenever the process behavior deviates significantly from the established parameters. The Model Parameter Estimator outputs the value of the calculated process model parameters, the statistical residual between the actual data and the calculated model and an indication of the parameters estimate quality.



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### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N + 1 2 N + 4 N N N N N N N N N N N N N N N N N	REAL REAL REAL REAL BOOLEAN	Model Parameter A Model Parameter B Model Parameter C Residual Quality of Model Parameter Estimates (0 = Good, 1 = Bad)

SPEC. NO.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1	МО	5	INT(2)	0 to 255	Block address of controlled process variable
S2	NO	5	INT(2)	0 to 255	Block address of control output
\$3	NO	Ö	INT(2)	0 to 255	Block address of Reset Trigger (Resets on 0 to 1 transition)
S4	YES	0 25	REAL(3)	0 25 to 9 2E18	Sample Time (seconds)
S5	YES	10	REAL(3)	0 25 to 9 2E18	Process Deadtime (seconds)
S6	YES	0 0	REAL(3)	0 0 to 9 2E18	Expected noise level in process variable (peak-to-peak)
S7 S8	YES NO	0 0 0	REAL(3) INT(2)	FULL 0 to 9998	Spare real parameter Spare boolean input



### ISC PARAMETER CONVERTER

### **GENERAL DESCRIPTION**

The ISC Parameter Converter function block calculates optimal tuning parameters for the associated Inferential Smith Controller (ISC) using the outputs of the Model Parameter Estimator. The tuning values are the process gain, process deadtime and process lag time. These outputs describe process dynamics at one operating point.

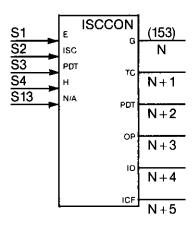
Through a direct link with the ISC, the tuning parameters may be directly adapted, however, they will only be adapted when

- 1 The appropriate adapt option is selected in S9 and
- 2 The quality output of the associated Model Parameter Estimator (FC 152) is good (zero)

The ISC Parameter Converter also supervises an automated initialization routine for establishing initial estimated for the associated ISC and Model Parameter Estimator After completion of initialization, the Converter tunes

- the ISC deadtime, gain and lag time
- the ISC tuning time constant
- the Minimum and Maximum Process Gain for the Converter (FC 153)
- the Minimum and Maximum Process Lag Time for the Converter
- the Sample Time and Expected Noise Level for the Model Parameter Estimator (FC 152)

The ISC Parameter Converter also updates the estimated process deadtime for the associated ISC and Model Parameter Estimator whenever input S3 is connected to a function block other than number 5, and the initialization trigger equals zero. If the above is not true, the ISC Parameter Converter updates the Model Parameter Estimator with the value being used by the ISC.



### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Estimated Process Gain
N + 1	REAL	Estimated Process Time Constant
N + 2	REAL	Adjusted Process Deadtime
N + 3	REAL	Estimated Process Operating Point
N + 4	REAL	Initialization Output 0 = initialization com-
N + 5	BOOLEAN	plete/not in progress  1 = initialization failed  2 = initialization in progress Initialization complete flag pulsed to one after comple- tion of automated initializa- tion routine, then to zero after five cycles

SPEC. NO.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1	NO	5	INT(2)	0 to 9998	Block address of associated Model Parameter Estimator
S2	NO	5	INT(2)	0 to 9998	Block address of associated ISC Block address for deadtime
S3	NO	5	INT(2) INT(2)	0 to 9998 0 to 9998	Block address of hold signal
S4 S5	NO   YES	-9 2E18	REAL(3)	FULL	Minimum allowable value for process gain
S6	YES	9 2E18	REAL(3)	FULL	Maximum allowable value for process gain
S7	YES	00	REAL(3)	0 0 to 9 2E18	Minimum allowable value for process lag time
S8	YES	9 2E18	REAL(3)	0 0 to 9 2E18	Maximum allowable value for process lag time
S9	NO	0	INT(2)	0 to 3	Adapt Option
				1	0 = no adapt
					1 = adapt process gain only 2 = adapt lag time only
	'		!		3 = adapt lag time only 3 = adapt both process gain and lag time
640	VEC	0	INT(1)	0 to 1	Initialization trigger (on 0 to 1 transition)
S10 S11	YES	50	REAL(3)	FULL	Maximum control output change for initialization
S12	YES	00	REAL(3)	FULL	Spare real parameter
S13	NO	١٥٥	INT(2)	0 to 9998	Spare boolean input

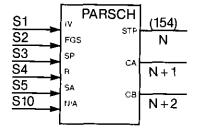
### ADAPTIVE PARAMETER SCHEDULER

### **GENERAL DESCRIPTION**

The Adaptive Parameter Scheduler function allows process characteristics such as a measured or calculated index variable to be used to adjust the tuning parameters for the associated Inferential Smith Controller (ISC) (FC 160). This feature optimizes controller performance for predictable changes in process operation and prevents periods of potentially unacceptable control while the ISC is being retuned by the Model Parameter Estimator via the ISC Parameter Converter.

The Adaptive Parameter Scheduler can be used to automatically establish the relationship between an ISC tuning parameter and a measured or calculated index variable using linear regression. The Adaptive Parameter Scheduler uses this relationship to automatically adjust the specified ISC tuning parameter based on the value of the specified index variable.

Alternatively, this function can be used to automatically determine the correction bias required for a pre-established gain schedule. This permits a nonlinear relationship to be established between the ISC tuning parameter and the index variable, with automatic correction of the relationship for design inaccuracies and/or changes in process behavior.



### **OUTPUTS**

BLOCK NUMBER	DATA TYPE	DESCRIPTION
N	REAL	Scheduled Tuning Parameter
N + 1	REAL	Coefficient A of Correction Equation
N + 2	REAL	Goefficient B of Correction Equation

SPEC. NO	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
 S1	NO	5	INT(2)	0 to 9998	Block address of index variable
S2	NO	5	INT(2)	0 to 9998	Block address of fixed gain schedule
S3	NO	5	INT(2)	0 to 9998	Block address of scheduled parameter
S4	NO	Ō	INT(2)	0 to 9998	Block address of reset trigger
S5	NO	5	INT(2)	0 to 9998	Block address of spec to be adapted
S6	NO	Ō	INT(1)	0 to 255	Spec to be adapted
S7	NO	0 0	REAL(3)	FULL	Minimum index value
S8	NO I	0 0	REAL(3)	FULL	Maximum index value
S9	NO	0	INT(2)	0 to 9998	Block address of Hold/Update Coefficient Flag 0 = Update A, B 1 = Hold Update of A, B
S10	NO	5	INT(2)	0 to 9998	Spare real input

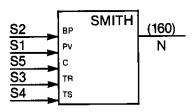
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### **FUNCTION CODE 160**

### **SMITH PREDICTOR**

### **GENERAL DESCRIPTION**

The SMITH PREDICTOR Function Code provides predictive process control on an error signal developed for the process variable and set point inputs measured against an internal model of the process. It is used for processes that are difficult to control with a PID controller because of long process dead times. The output is limited by operator specified high and low limits, and the block can be forced to follow an external value.



### **OUTPUTS**

BLOCK Number	DATA TYPE	DESCRIPTION	
N	REAL	Predictive control value	

SPEC.	TUNE	DEFAULT VALUE	DATA TYPE	RANGE MINIMUM MAXIMUM	DESCRIPTION
S1	NO	0	INT	0 to 255	Block address of process variable
S2	NO	0	INT	0 to 255	Block address of set point
S3	NO	0 5	INT	0 to 255	Block address of track reference value
S4	NO	0	INT	0 to 255	Block address of track reference flag 0 = track 1 = release
S5	NO	5	INT	0 to 255	Block address of external reference value (cascade)
S6	NO	0	BOOLEAN	0 or 1	Use external reference flag 0 = Normal 1 = use
S7	YES	1 000	REAL(3)	FULL	Process gain
S8	YES	0 000	REAL(3)	0 0 to 9 2 E 18	Process dead time (seconds)
S9	YEŞ	0 000	REAL(3)	0 0 to 9 2 E 18	Process lag time constant (seconds)
S10	YES	0 000	REAL(3)	FULL	Process tuning time constant
S11	YES	100 000	REAL(3)	FULL	Output high limit
S12	YES	0 000	REAL(3)	FULL	Output low limit



### **EXPLANATION**

A SMITH PREDICTOR is used to control processes that have long time delays. For example, assume a control system is to maintain a certain property at the end of a 1000 foot paper machine by adjusting its inlet composition. There will be a delay between a control action being taken and the result of that action being measured at the end of the machine because the system has no way of waiting through the deadtime to determine the effect the control action had on the process. This causes problems for PID controllers, since they have no way of waiting 20 seconds, or four minutes, or whatever the delay may be, to see if the control action they took was correct. Sluggish tuning is required on this type of process.

The functionality of the inferential SMITH PREDICTOR block is shown in the block diagram of Figure 160-1. The block compares the process value (PV) to the model value (MV) from the internal model. The controller responds to set point changes and differences between the PV and MV. The filter time constant allows the user to adjust the speed of response, the smaller the time constant, the quicker the time response.

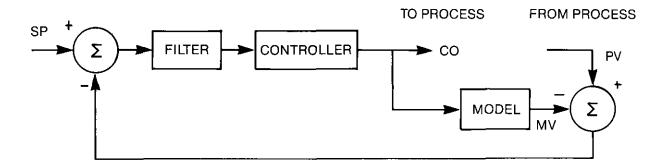
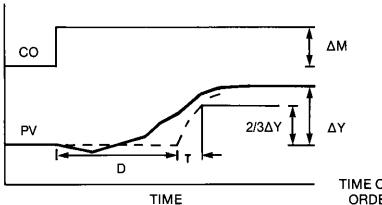


FIGURE 160-1 — Functionality of the SMITH PREDICTOR Function Block

In order to determine the specifications for the model, a simple step response test can be performed. Figure 160-2 illustrates the procedure for finding the model parameters.



**INPUT TO PROCESS** 

PROCESS RESPONSE AND FIRST ORDER MODEL

$$GAIN = \frac{\Delta Y}{\Delta M}$$

TIME CONSTANT = T, TIME FOR 1ST ORDER MODEL TO REACH 2/3 ΔΥ

DEAD TIME = D, TIME FOR Y TO RESPOND AFTER CHANGE IN M

FIGURE 160-2 — Determining Model Parameters From a Step Input

Several step responses should be obtained from the process. If the model parameters are consistent, the filter time constant may be made small. A very fast response would be obtained by setting the filter constant equal to one third of the model time constant. If the model is uncertain, the filter time constant should by set equal to the uncertainty in the deadtime. An alternate method of tuning is to set the filter time constant to the deadtime plus the model time constant. Perform set point changes and successively reduce the filter time constant until a desirable response is obtained.

### **SPECIFICATIONS**

S1 - PV - Block address of process variable

S2 - SP - Block address of set point

S3 - TRACK - Block address of track reference value. The set point will track the value in this block when the track switch signal is a 0.

\$4 - SWITCH - Block address of track switch signal. The set point will track <\$5 > when this input is a 0.

0 = Track

1 = Release

\$5 - REFER - Block address of an external reference value. This is a Cascade input with no connections to the SMITH PREDICTOR block. This value can be used to force the output to a safe value in case of equipment failure. If it is not in use then \$5 should reference the same block as \$2.

- S6 RFLAG Block address of the external reference flag. If this input is a 1, then the set point will track the external reference value
  - 0 = Release
  - 1 = Track reference value
- S7 GAIN Process model gain This is used with S9 to create an ideal process model. This value is defined for the ideal process with no dead time.
- S8 DEADT Process dead time. This value identifies the actual dead time in the real process. In most cases with will be a fixed value. In other cases, it may change with the process. When this occurs, it may be necessary to modify S8 with an ADAPT block to reflect actual changes in the dead time.
- S9 LAGT Process model lag time This is used with S7 to create an ideal process model. It is defined for the ideal process with no dead time.
- S10 TUNET The tuning time constant is used to take into account the performance characteristics of different processes. A good starting value is about 1.3 times the process dead time.
- S11 HIGH High output limit This will normally be 105 0
- S12 LOW Low output limit This will normally be -50

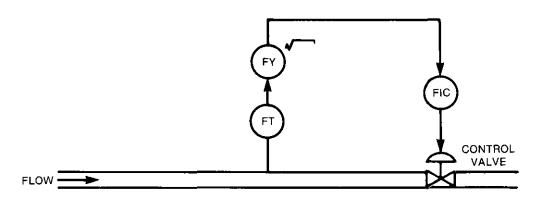
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### BASIC CONTROL LOOP

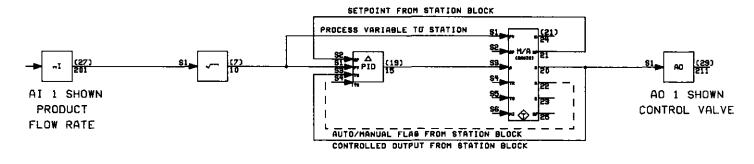
The following example uses a Basic Station combined with a PID controller to form a typical control loop. The application shown requires a regulated flow, where the flow is measured using a differential pressure transmitter and regulated using a control valve.

To implement the control on the Loop Command Controller, the differential pressure signal is brought in through one of the Analog Inputs and connected to a square root function to calculate the Process Variable flow rate (in engineering units). This PV and the setpoint signal from the station (which is driven by a CLC under operator control) are connected to the PID controller and the output of the PID is the Auto input to the station. The Control Output signal from the station is connected to an Analog Output to drive the valve. When the station is in the Auto Mode the operator can adjust the setpoint and PID will have control of the CO signal. If the station is put into Manual Mode the operator can control the CO signal directly. In this mode the PID is forced to track the CO signal as a track reference. The M/A status flag is connected to the track switch of the PID to initiate this action. This will cause the PID to track the CO signal when in Manual Mode and the transfer to Auto will therefore be bumpless.

### BASIC CONTROL LOOP



### LOOP COMMAND FUNCTION BLOCKS



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Solid lines on the Loop Command Function Block drawings indicate analog signals and dashed lines indicate boolean signals

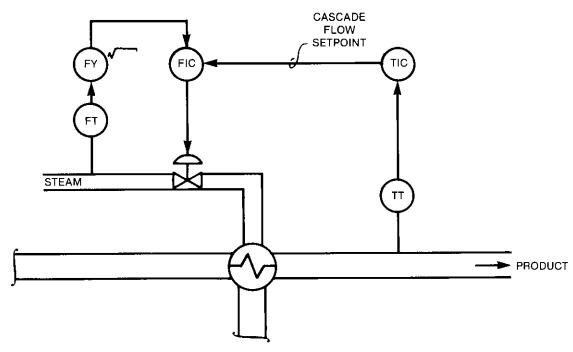
### CASCADE CONTROL LOOP

A Cascade control structure is shown next. In this structure the output of the primary controller is used as a setpoint to the secondary controller. Each controller has its own measurement value but only the secondary controller has a control output signal. The secondary controller in this structure may be operated separately from the primary or put into cascade operation where its setpoint is determined by the primary controller.

The Loop Command Controller implementation uses two Analog Inputs for the two measurements, two PID controllers, a Basic station for the primary loop for display of and adjustment of the primary process variable and setpoint and a Cascade station for mode selection, display and manual adjustment of the secondary process variable and setpoint Display and manual adjustment of the analog output signal is also provided. Note that the secondary station may be operated in Manual, Auto or Cascade Mode. In Cascade Mode the secondary controller will be in automatic. To prevent windup at the primary controller, the cascade state flag is used to force the primary controller to track the setpoint of the secondary loop until the secondary is put under Cascade control. Tracking by the secondary controller is the same as the standard feedback loop in Manual Mode.

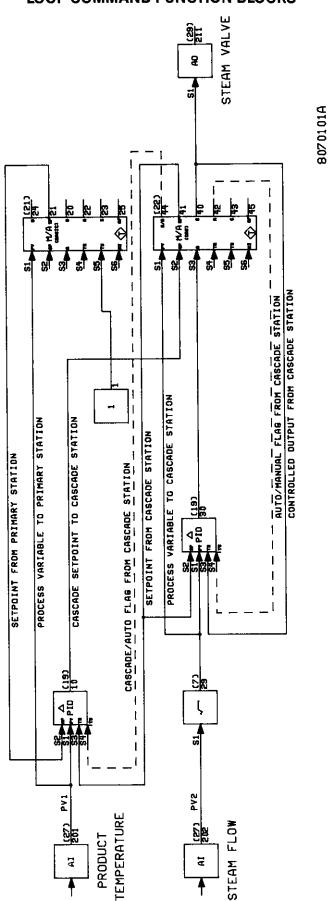
Reset windup can occur in any system, but most commonly in batch control systems where controllers may be monitoring control variables but not performing any control action during the current step. The controller will receive the signal, take action to correct the error, see no result, and take action to correct the error again. As long as the controller receives no results from its control action, it will continue to try to correct the error. When the controller is later called into service on some other step of the process, it will be wound up so far beyond the value of the controlled variable that it will not be able to control it.

### CASCADE CONTROL LOOP



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### LOOP COMMAND FUNCTION BLOCKS

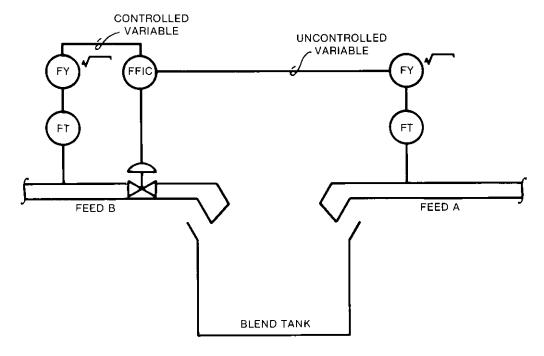


### RATIO CONTROL LOOP

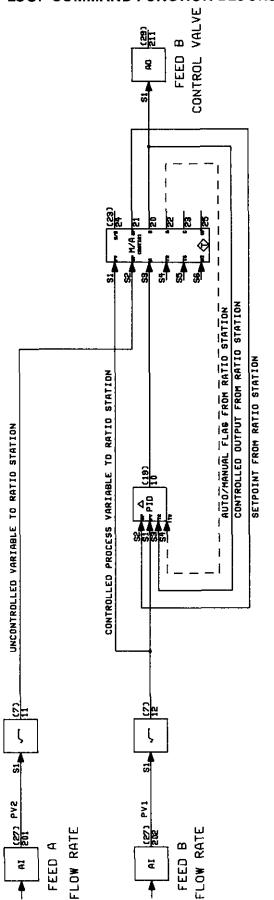
In a Ratio Control structure the objective is to control the ratio of two variables. The most common application of ratio control is in mixing operations. In general, a valve is used to control one process variable and the other variable is left uncontrolled or "wild". The operator selects the desired ratio and the setpoint if the controlled variable needed to maintain the ratio is determined from the ratio multiplied by the "wild" variable.

The control structure for the Loop Command Controller uses two analog inputs for PV, and PV<sub>2</sub>, and the PID function, a Ratio Station and an Analog output for the control output. The station may be operated in Manual Mode, where the control output is directly controlled, Auto Mode where the operator may set the setpoint or in Ratio Mode where the operator selects the ratio value and the station calculates the setpoint as the ratio times the PV<sub>2</sub> value. The tracking structure for Manual Mode is the same as that used for the basic feedback loop. Note that Ratio control could be implemented without a special station using a multiply block but the direct control of the ratio value and the need to display the actual setpoint require that these values be available to the operator interface devices. Bumpless transfer of setpoint is achieved by computing the actual ratio whenever the station is not in Ratio Mode.

### RATIO CONTROL LOOP



### LOOP COMMAND FUNCTION BLOCKS

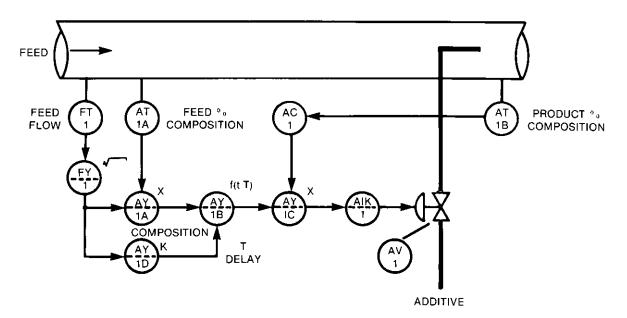


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### **ANALOG TIME DELAY**

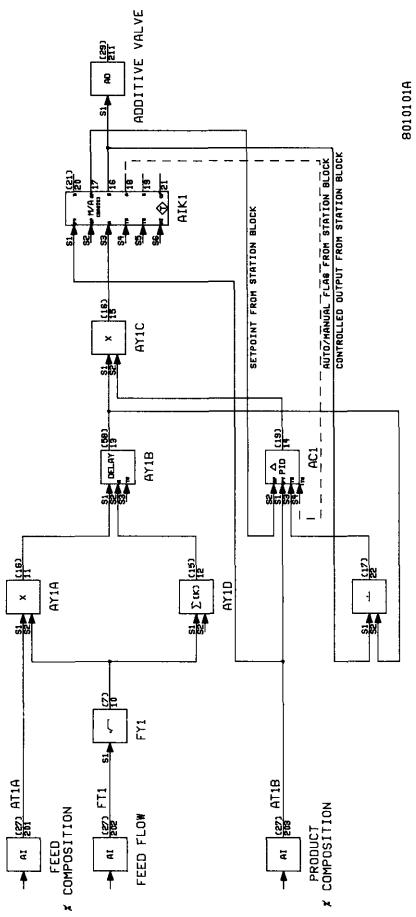
The Analog Time Delay example involves the inline blending of two streams where the feedforward index is determined a considerable distance upstream of the additive stage, thus resulting in an apriori knowledge of feed composition. Assuming plug flow and a fixed pipe dimension, the process transport time as a function of feed flow can be computed. A variable analog time delay is therefore used where the upstream mass flow composition is delayed. T seconds prior to being used as a feedforward index to the final regulatory loop.

### ANALOG TIME DELAY — BLENDING EXAMPLE



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### LOOP COMMAND FUNCTION BLOCKS



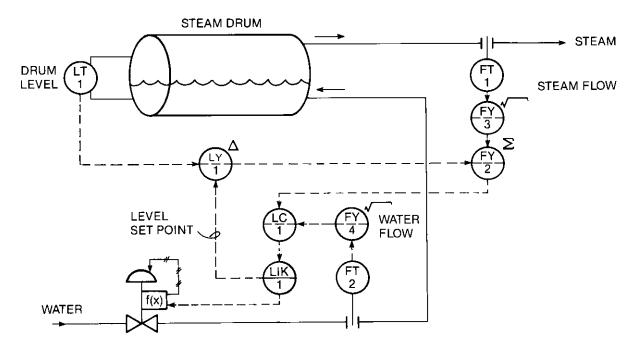


### THREE ELEMENT FEEDWATER CONTROL

A Three Element Feedwater Control system is designed to provide a continuous mass balance, since for every pound of steam generated and removed from the boiler, a pound of water must be added to replace it. An unbalance in this relationship will result in a change in drum level

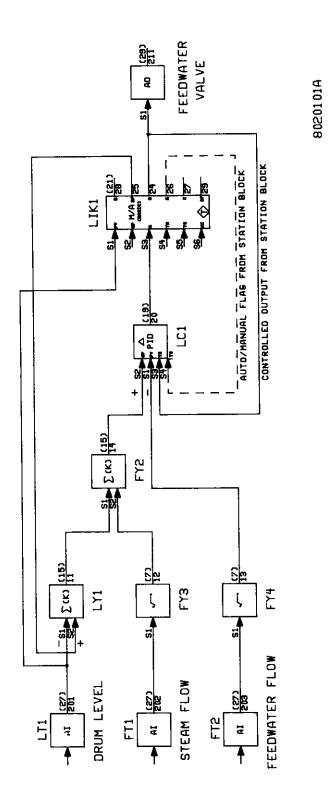
For this reason, the steam flow measurement is used as a feedforward load index in determining feedwater demand. This feedforward demand is in turn recorrected, based on drum level deviation from set point and used as the cascaded set point for the feedwater controller.

### THREE ELEMENT FEEDWATER CONTROL



### 23:11:14 04/10/07

### LOOP COMMAND FUNCTION BLOCKS



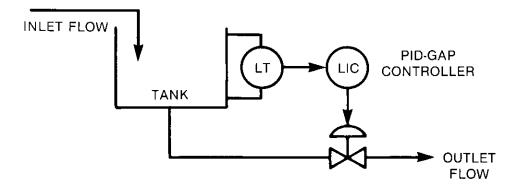


### PID — GAP CONTROL

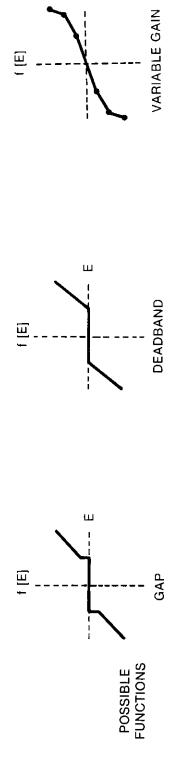
### And Generalized Error Characterization

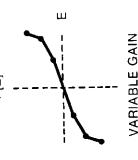
There are a number of applications where linear control response to an error signal is undesirable. For example, if the design objective of your tank level control is to stabilize output flow to a downstream process unit then a form of Gap control is desirable. Gap control will dampen out the effect of upstream fluctuations in flow by letting the tank level vary within a prespecified range. Large upstream fluctuations will result in control action to maintain tank level at the setpoint.

PID — Gap control is implemented on the Loop Command Controller by computing the error between the process variable and the setpoint outside the PID control algorithm. The error signal is then shaped by a function generator function code. Typical shapes as well as the function block configurations are shown on the following pages.

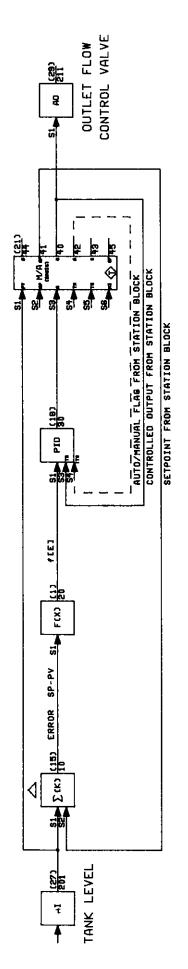


# ERROR CHARACTERIZATION USING A FUNCTION GENERATOR ON ERROR





# **LOOP COMMAND FUNCTION BLOCKS**



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### FEEDFORWARD CONTROL

Feedforward control is a control technique that calculates an output based on process measurements, the desired setpoint and a model of the process. Since it is difficult to get a totally accurate process model, feedforward control is often used with a feedback loop to correct the setpoint to take into account modeling errors and unmeasured process disturbances.

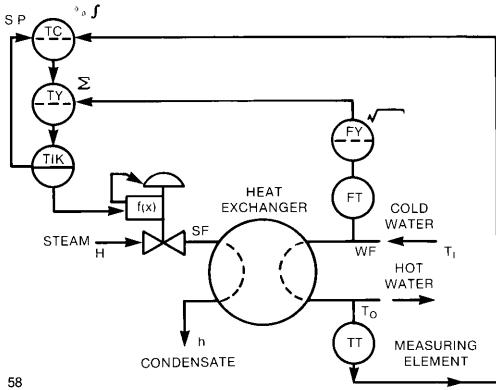
There are many variations of feedforward control but three typical configurations are included, each containing varying levels of model complexity. The first two examples are associated with a process heat exchanger. The third example is a density control loop associated with an evaporator.

The two process heat exchanger control configurations are examples of steady state feedforward control. The feedforward process model is designed to compensate for the inherent nonlinearities associated with heat exchangers over their operating range.

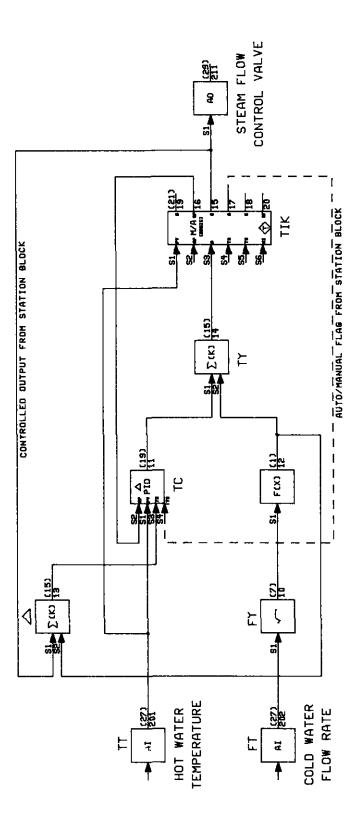
The first process heat exchanger example assumes that steam and cold water temperatures and pressures are relatively constant. Under these conditions, water flow can be used to infer steam valve position demand such that the desired exit hot water temperature can be achieved. The closed loop temperature controller will bias the steam valve position demand in response to transient disturbances and steady state regulation of water temperature.

The Loop Command Controller implementation includes a function generator in the feedforward demand. A feedforward program of water flow as steam valve demand will be entered to linearize process characteristics for the feedback controller. It has been assumed for this example that gain scheduling of the controller was not required.

# TEMPERATURE CONTROL OF A PROCESS HEAT EXCHANGER (FIRST EXAMPLE)



### LOOP COMMAND FUNCTION BLOCKS

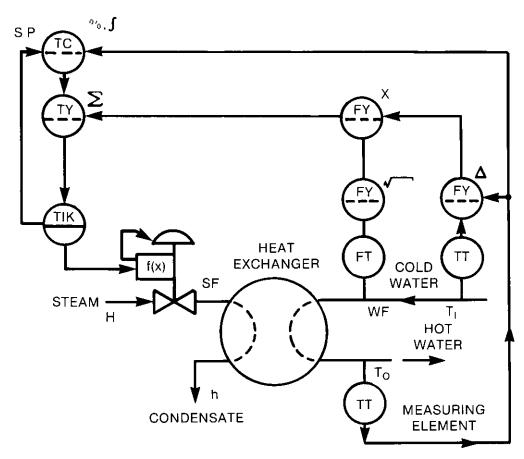


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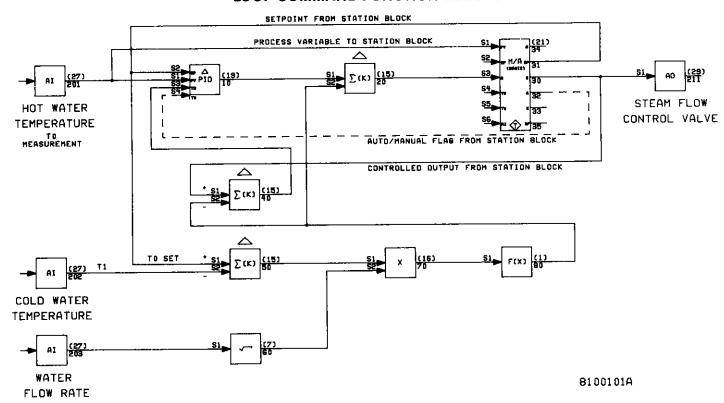
The second process heat exchanger example shows an alternative configuration for the feedforward control loop that accounts for both cold water temperature and desired hot water temperature and flow rate. These three parameters are used to estimate energy requirements for the heat exchanger. This estimate will be used to infer steam valve position demand using a function generator such that the desired exit hot water temperature can be achieved. The closed loop temperature controller will bias the steam valve position demand in response to transient disturbances and steady state regulation of water temperature. The steam valve can be controlled manually using the Auto/Manual station. Bumpless transfer is incorporated into the track reference signal to the PID controller.

# TEMPERATURE CONTROL OF A PROCESS HEAT EXCHANGER (SECOND EXAMPLE)



### 23:11:20 04/10/07

### LOOP COMMAND FUNCTION BLOCKS



The third example is the product density control of an evaporator. This control utilizes an Inferential Smith Predictor as the primary controller and a dynamic feedforward compensation circuit to decouple the primary controller from changes in product density flowrate. The secondary controller consists of a PID algorithm to maintain the steam flow rate at setpoint.

The dynamic feedforward control strategy is based on the ratio of the two transfer function models that estimate the change in density caused by a change in product flow rate and steam flow rate. For example, if the steam flow to density transfer function can be approximated as

$$Gs = \frac{Ks (e)^{-TsS}}{TsS + 1}$$

and product flow to density transfer function can be approximated as

$$Gp = \frac{Kp (e)}{TsS + 1}$$

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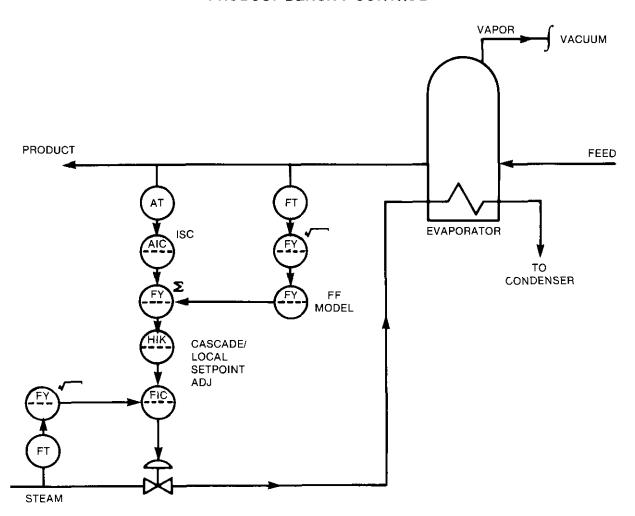
then the feedforward transfer function is

Gff = 
$$\frac{-Gp}{Gs}$$
  
=  $\frac{-Kp}{Ks}$  •  $\frac{Ts S + 1}{Tp S + 1}$  • (e)  $-(Tp - Ts)S$ 

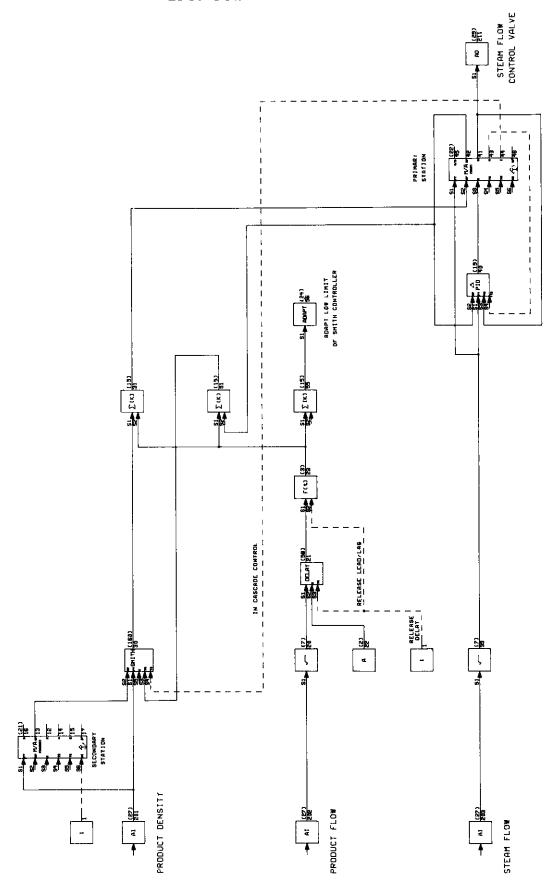
where K = Gain, T = Time constant, T = DeadtimeThe above feedforward model assumes that Tp is greater than Ts

In the Loop Command Controller the primary/secondary faceplate display option is used. The secondary faceplate display is used to display product density and its setpoint. The primary faceplate is the Cascade/Auto/Manual station.

### PRODUCT DENSITY CONTROL



### LOOP COMMAND FUNCTION BLOCKS



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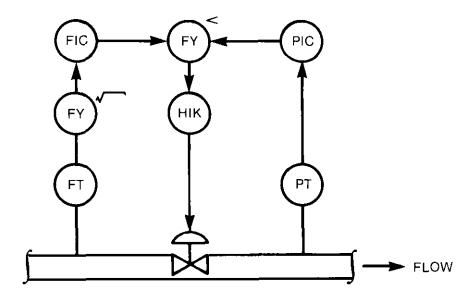
### **OVERRIDE CONTROL**

Override control systems are used where two or more variables must not exceed certain limits for reasons of safety or economy. Next is an example of a control system where it is normally desired to control the product flow. If the downstream pressure approaches a high limit then to protect the equipment the product flow rate will be reduced to prevent excessive pressure. This is done by selecting the lower of the outputs from the flow control loop or the pressure control loop.

In this example, a standard control loop with a station is used for flow, a standard control loop is used for the pressure limit and a low select to determine the valve position demand. To prevent the controller that is not selected from winding up, the output of the low select is used to clamp the high limits of both PID controllers.

The flow controller faceplate is also used for manual adjustment of the flow control valve

### **OVERRIDE CONTROL**



# LOOP COMMAND FUNCTION BLOCKS 8 PRIMARY STATION SECONDARY Station SETPOINT TO CONTROLLER 20 00 E PROCESS VARIABLE TO STATION HOMPT (1243) 400PT (291) PROCESS VARIABLE TO STATION SETPOINT TO CONTROLLER St. (115) DOWNSTREAM PRESSURE PRODUCT FLOW RATE 77 #

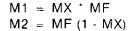
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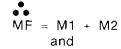
### DECOUPLED BLENDING CONTROL

In many control situations process variables are "coupled" in the same sense that a change in a manipulated variable that affects one process variable will also affect the other Decoupling Control systems attempt to reverse the process model to allow the operator to adjust one variable without affecting other variables in the system. The process is a blending process and it is desired to control the total flow and the composition by controlling the flow of the two ingredients  $m_1$  and  $m_2$ . Since the total flow is given by the sum of the two ingredient flows and the composition is given by the ratio of one ingredient to the total flow,  $m_1$  and  $m_2$  can be solved for in terms of  $m_f$ , the desired total flow, and  $m_\chi$  the desired composition

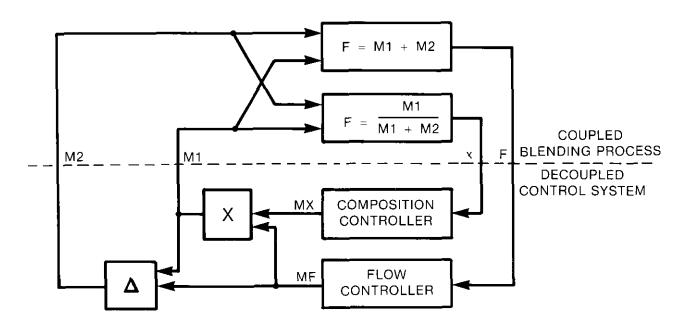
In this example, we have two basic feedback loops, each using a PID and Station, a multiply block to calculate m<sub>1</sub> and a difference block to determine m<sub>2</sub> Note that any model that can be expressed in terms of add, subtract, multiply and divide may be easily implemented in the module

### **DECOUPLED BLENDING CONTROL**



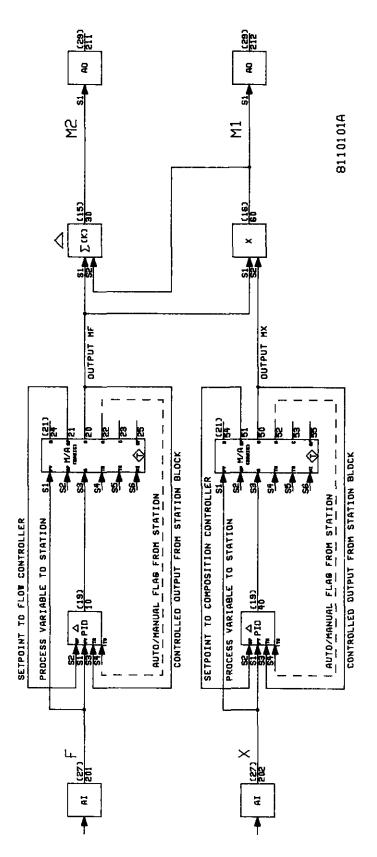


$$MX = \frac{M1}{M1 + M2}$$



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### LOOP COMMAND FUNCTION BLOCKS



### SELF-TUNING CONTROL

Many industrial processes are now required to perform efficiently over a wide range of operating conditions. In many cases, these processes and their control systems were initially designed to produce a single product at a single production rate. Current economic conditions often require the same process to produce a variety of products at a variety of production rates. In many cases, the necessary operating efficiencies require major changes in both the process design and the control strategy.

However, one fundamental problem continues to limit process performance Conventional process controllers cannot effectively control the required variables over a broad range of process operating conditions. Many techniques address this problem, but only with limited success. Bailey Controls provides a unique self-tuning control capability which combines the attributes of many of these techniques, and overcomes the problems associated with each. The most effective elements of modern control theory, estimation theory and numerical analysis have been combined with a solid base of process control experience to develop this self-tuning control capability.

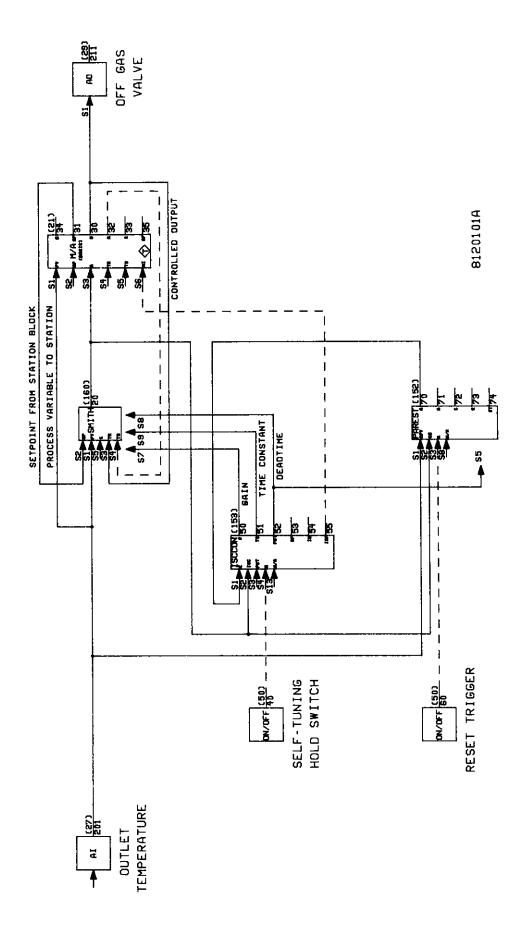
A group of specialized function blocks have been developed to provide selftuning for the Inferential Smith Controller (ISC) algorithm available in Bailey microprocessor-based controllers. These function blocks can be configured into the control logic to provide superior control for industrial processes which must perform efficiently over a wide range of operating conditions.

The Model Parameter Estimator monitors the controlled process variable and control output for the ISC, and automatically establishes a first-order dynamic model of these variables. The parameters of this dynamic model are automatically translated to the required controller tuning parameters by the ISC Parameter Converter. For processes where ISC tuning parameters are related to other process variables, an Adaptive Parameter Scheduler automatically establishes a statistically valid correlation and adjusts the tuning parameters for the ISC based on this correlation.

For a detailed explanation of the Bailey Self-Tuning algorithm, please refer to Application Guide AG-0000-953-01

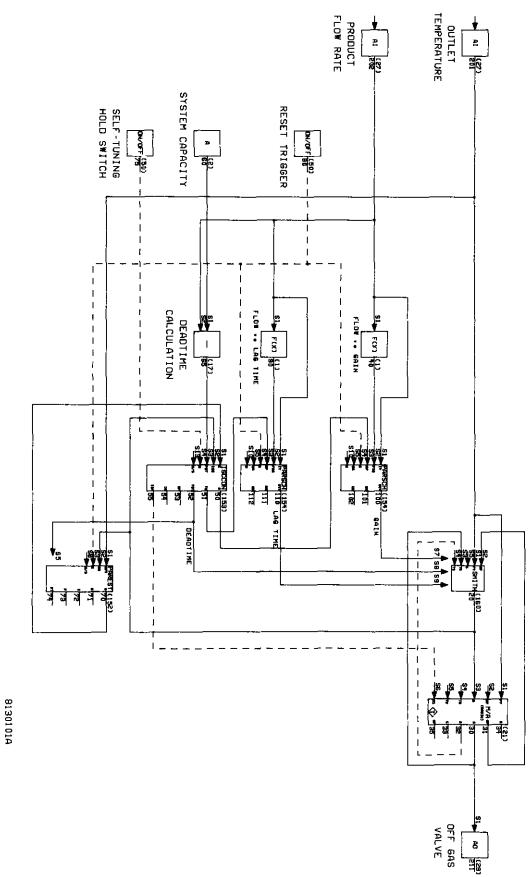
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### **BASIC SELF-TUNING CONFIGURATION**



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# ADVANCED SELF-TUNING CONFIGURATION WITH DEAD TIME SCHEDULING AND ADAPTIVE GAIN/LAG SCHEDULING



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### **REFERENCES:**

TECHINCAL PAPER TP81-7

"Using a Building Block Approach to Implement Advanced Control Technique" K L King

TECHNICAL PAPER TP79-3

"Analog Control Techniques and Tuning" RK Johnson

APPLICATION GUIDE AG-E93-900-1

"Three Element Feedwater Control"

APPLICATION GUIDE AG-E93-900-4

"Analog Time Delay"

APPLICATION GUIDE AG-0000-953-01

"Self-Tuning Control"

